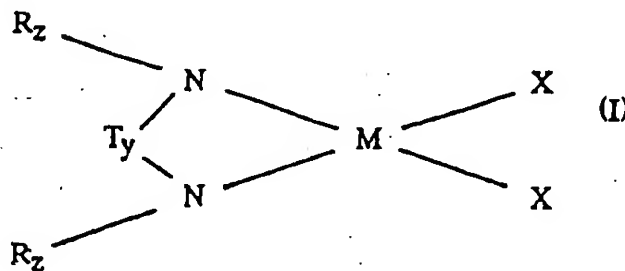




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<b>(21) International Application Number:</b> PCT/US91/09676 <b>(22) International Filing Date:</b> 26 December 1991 (26.12.91) <b>(30) Priority data:</b> 634,987 27 December 1990 (27.12.90) US <b>(71) Applicant:</b> EXXON CHEMICAL PATENTS INC. [US/US]; 1900 East Linden Avenue, Linden, NJ 07036-0710 (US). <b>(72) Inventors:</b> CANICH, Jo, Ann, Marie ; 900 Henderson Avenue #808, Houston, TX 77058 (US). TURNER, Howard, William ; 4318 Misty Heather Court, Houston, TX 77059 (US).		<b>(74) Agents:</b> BUTTS, Evan et al.; Exxon Chemical Company, P.O. Box 5200, Baytown, TX 77522-5200 (US). <b>(81) Designated States:</b> AT (European patent), AU, BE (European patent), BR, CH (European patent), DE (European patent), DK (European patent), ES (European patent), FI, FR (European patent), GB (European patent), GR (European patent), HU, IT (European patent), JP, KR, LU (European patent), MC (European patent), NL (European patent), NO, PL, RU, SE (European patent). <b>Published</b> <i>With international search report.</i>

**(54) Title:** AN AMIDO TRANSITION METAL COMPOUND AND A CATALYST SYSTEM FOR THE PRODUCTION OF ISOTACTIC POLYPROPYLENE

**(57) Abstract**

Bridged and unbridged amido transition metal compounds of the Group IV-B metals are disclosed. They are represented by general formula (I) wherein: "y" is 1 denoting the presence of a bridging group T between nitrogen atoms; "Z" is - y; "M" is zirconium, hafnium or titanium; "N" is a nitrogen atom having three substituents; each "X" is, independently, any univalent anionic ligand such as a halide, hydride, substituted or unsubstituted C<sub>1</sub>-C<sub>30</sub> hydrocarbyl, alkoxide, aryloxy, amide, arylamide, phosphide, or arylphosphide; "T" is a covalent bridging group selected from the group consisting of unsubstituted hydrocarbyl and substituted hydrocarbyls containing a Group IV-A or VI-A element; and each "R" is, independently, a radical selected from the group consisting of singly branched hydrocarbyl radicals having between 4 and 30 carbon atoms, multiply branched hydrocarbyl radicals having between 4 and 30 carbon atoms, halogen radicals, amido radicals, phosphido radicals, silyl radicals, alkoxy radicals, alkylborido radicals, C<sub>1</sub>-C<sub>30</sub> hydrocarbyl-substituted Group IV-A metalloid radicals; and substituted C<sub>1</sub>-C<sub>30</sub> hydrocarbyl radicals wherein one or more hydrogen atoms is replaced by a halogen radical, an amino radical, a phosphido radical, an alkoxy radical or any other radical containing a Lewis acidic or basic functionality. These compounds may be used in a catalyst system comprising the amido transition metal compound and an alumoxane. Also disclosed is a process using the catalyst system for the production of high molecular weight polyolefins and, particularly, high molecular weight isotactic polypropylene.

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AN AMIDO TRANSITION METAL COMPOUND AND A  
CATALYST SYSTEM FOR THE PRODUCTION OF  
ISOTACTIC POLYPROPYLENE.

SPECIFICATION

FIELD OF THE INVENTION

5 This invention relates to certain bridged and  
unbridged amido transition metal compounds of the Group  
IV-B metals, to a catalyst system comprising an amido  
transition metal compound and an alumoxane, and to a  
process using the catalyst system for the production of  
10 high molecular weight polyolefins and, particularly, high  
molecular weight isotactic polypropylene.

BACKGROUND OF THE INVENTION

15 The various compounds that are derived from the  
polymerization of  $\alpha$ -olefins show huge differences in  
their chemical and physical properties. These  
differences reflect differences in molecular structure,  
some of which are inherent in the use of a particular  
monomer or monomer combination, and some of which result  
20 from a pattern, or lack thereof, in how the monomers are  
combined. It is inherent that polymers of  $\alpha$ -olefins  
having 3 or more carbon atoms will have pendant  
hydrocarbyl groups attached to the polymer backbone chain.  
However, the stereochemical arrangement of these  
hydrocarbyl groups is a consequence of the interaction of  
25 monomer, catalyst and coordinated polymer during  
polymerization. Any pendant hydrocarbyl group may be  
said to lie on one side of a plane defined by the carbon  
atoms of the polymer backbone in an idealized elongated  
configuration.

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As previously alluded to, the physical properties exhibited by a particular olefin polymer of a particular molecular weight are determined in major part by the arrangement of these hydrocarbyl groups along the polymer backbone. Strong polymers tend to be stereochemically regular, meaning the adjacent hydrocarbyl groups reside on the same side of the polymer backbone or switch at fairly regular intervals. Either arrangement facilitates crystallization thus lending rigidity and strength to the solidified polymer.

Other critical determinants of the properties which a polymer will exhibit are the type and relative concentration of monomers and comonomers, the weight average molecular weight ( $M_w$ ) of the polymer molecules comprising the resin bulk, the molecular weight distribution (MWD) and the composition distribution of the resin. For end use applications which require high strength and low creep, the  $M_w$  of such a resin must generally be in excess of 100,000.

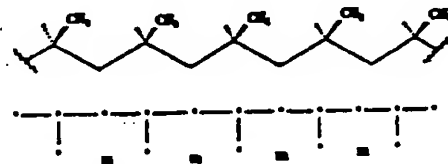
Five types of stereoregularity, or tacticity, have been characterized: atactic, normal isotactic, isotactic stereoblock, syndiotactic, and hemiisotactic. Although all of these stereoregular configurations have been primarily demonstrated in the case of polypropylene, in theory each is equally possible for polymers comprised of any olefin, cyclic olefin or internal olefin, having 3 or more carbon atoms.

Atactic polyolefins are those wherein the hydrocarbyl groups pendent to the polymer molecule backbone assume no regular order in space with reference to the backbone. This random structure is represented by a polymer backbone of alternating methylene and methine carbons, with randomly oriented branches substituting the methine carbons. The methine carbons randomly have R and S configurations, creating adjacent pairs either of like

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configuration (a "meso" or "m" dyad) or of unlike configuration (a "racemic" or "r" dyad). The atactic form of a polymer contains approximately equal fractions of meso and racemic dyads. Since atactic polyolefins exhibit no regular order or repeating unit configurations in the polymer chain, they are amorphous materials. Atactic polyolefins exhibit little if any crystallinity, hence they are generally unsuitable for high strength applications regardless of the weight average molecular weight of the resin.

Isotactic polyolefins are those wherein the pendent hydrocarbyl groups are ordered in space to the same side or plane of the polymer backbone chain. Using isotactic polypropylene as an example, the isotactic structure is typically described as having the pendent methyl groups attached to the ternary carbon atoms of successive monomeric units on the same side of a hypothetical plane through the carbon backbone chain of the polymer, e.g., the methyl groups are all above or below the plane as shown below.



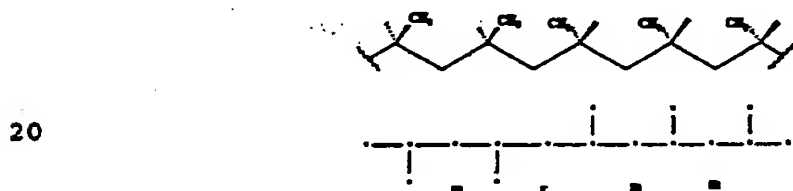
The degree of isotactic regularity may be measured by NMR techniques. Bovey's NMR nomenclature for an isotactic pentad is ... mmmm ... with each "m" representing a "meso" dyad or successive methyl groups on the same side in the plane.

In the normal isotactic structure of a polyolefin, all of the monomer units have the same stereochemical configuration, with the exception of random errors which appear along the polymer. Such random errors almost always appear as isolated inversions of configuration which are corrected in the very next  $\alpha$ -olefin monomer

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insertion to restore the original R or S configuration of the propagating polymer chain.

The formation of stereoblock isotactic polymer differs from the formation of the normal isotactic structure in the way that the propagation site reacts to a stereochemical error in the chain. As mentioned above, the normal isotactic chain will return to the original configuration following an error because the stereochemical regulator, the catalytic active metal species and its surrounding ligands, continues to dictate the same stereochemical preference during monomer insertion. In stereoblock propagation, the catalytically active metal site itself changes from one which dictates a monomer insertion of R configuration to one which dictates an S configuration for monomer insertion. The isotactic stereoblock form is shown below.



Long before anyone had discovered a catalyst system which produced the isotactic stereoblock form of a polyolefin, the possible existence of a polymer of such micro-structure had been recognized and mechanisms for its formation had been proposed based on conventional Ziegler-Natta mechanisms in Langer, A.W., Lect. Bienn. Polym. Symp. 7th (1974); Ann. N.Y. Acad. Sci. 295, 110-126 (1977). The first example of this form of polypropylene and a catalyst which produces it in a pure form were reported in U.S. Patent No. 4,522,982.

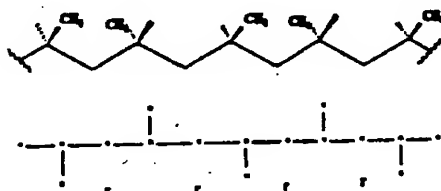
The lengths of individual blocks of the same configuration in the stereoblock structure vary widely due to changing reaction conditions. Since only the

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erroneous parts of the chains affect the crystallinity of the resin product, in general, normal isotactic polymers and isotactic stereoblock polymers of long block length (greater than 50 isotactic placements) have similar properties.

Highly isotactic polyolefins exhibit a high degree of crystallinity. Accordingly, isotactic polyolefins are, depending upon their weight average molecular weight exceeding about 100,000, well suited to high strength end use applications.

Syndiotactic polyolefins are those wherein the hydrocarbyl groups pendent to the polymer molecular backbone alternate sequentially in order from one side or plane to the opposite side or plane relative to the polymer backbone, as shown below.



In NMR nomenclature, this segment, or pentad, is described as ... rrrr ... in which each r represents a "racemic" dyad, i.e., successive methyl groups on alternate sides of the plane. The percentage of r dyads in the chain determines the degree of syndiotacticity of the polymer. Highly syndiotactic polymers are generally highly crystalline and will frequently have high melting points similar to their isotactic polymorphs. Like isotactic polyolefins, syndiotactic polyolefins are capable of exhibiting a high degree of crystallinity, hence are suitable for high strength applications provided their  $M_w$  exceeds about 100,000.

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For any of the above described materials the final resin properties and its suitability for particular applications depend on the type of tacticity, the melting point, the average molecular weight, the molecular weight distribution, the type and level of monomer and comonomer, the sequence distribution, and the presence or absence of head or end group functionality. Accordingly, the catalyst system by which such a stereoregular polyolefin is to be produced should, desirably, be versatile in terms of  $M_w$ , MWD, tacticity type and level, and comonomer choice. Further, the catalyst system should be capable of producing these polymers with or without head and/or end group functionality, such as olefinic unsaturation. Still further, such catalyst system must be capable, as a commercially practical constraint, of producing such resins at an acceptable production rate. Most preferably, the catalyst system should be one which, at its productivity rate, provides a resin product which does not require a subsequent treatment to remove catalyst residue to a level which is acceptable for the resin in the end use application desired. Finally, an important feature of a commercial catalyst system is its adaptability to a variety of processes and conditions.

Conventional titanium based Ziegler-Natta catalysts for the preparation of isotactic polymers are well known in the art. These commercial catalysts are well suited for the production of highly crystalline, high molecular weight materials. The systems are, however, limited in terms of molecular weight, molecular weight distribution, and tacticity control. The fact that the conventional catalysts contain several types of active sites further limits their ability to control the composition distribution in copolymerization.



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More recently a new method of producing isotactic polymers from an alumoxane cocatalyzed, or activated, metallocene which in its natural state has chirality centered at the transition metal of the metallocene, was reported in Ewen, J.A., J. Amer. Chem. Soc., v. 106, p. 6355 (1984) and Kaminsky, W., et al., Angew. Chem. Int. Ed. Eng.; 24, 507-8 (1985).

Catalysts that produce isotactic polyolefins are also disclosed in Patent No. 4,794,096. This patent discloses a chiral, stereorigid metallocene catalyst which is activated by an alumoxane cocatalyst which is reported to polymerize olefins to isotactic polyolefin forms. Alumoxane cocatalyzed metallocene structures which have been reported to polymerize stereoregularly are the ethylene bridged bis-indenyl and bis-tetrahydroindenyl titanium and zirconium (IV) catalyst. Such catalyst systems were synthesized and studied in Wild et al., J. Organomet. Chem. 232, 233-47 (1982), and were later reported in Ewen and Kaminsky et al., mentioned above, to polymerize  $\alpha$ -olefins stereoregularly. Further reported in West German Off DE 3443087A1 (1986), but without giving experimental verification, is that the bridge length of such stereorigid metallocenes can vary from a C<sub>1</sub> to C<sub>4</sub> hydrocarbon and the metallocene rings can be simple or bi-cyclic but must be asymmetric. In contrast to the metallocene catalysts disclosed in U.S. Patent No. 4,794,096 and West German Patent DE 3443087A1, certain species of this invention are capable of producing a highly isotactic polymer using an achiral catalyst.

The use of transition metal based catalysts having amido groups attached to the transition metal have received some attention in polymer research. A process for producing syndiotactic polystyrene using a tris-amido zirconium catalyst is disclosed in U.S. Patent No.

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4,774,301. As taught therein, the zirconium compound may be combined with an alumoxane to produce a polymerization catalyst. A syndiotactic polymer results when vinyl aromatic monomers, which have been known to yield syndiotactic polymers generally, are polymerized by a tris-amido zirconium-alumoxane catalyst.

In European Patent 349,886, titanium having bonded thereto a saturated alkyl-substituted amido group, is reported to yield an active catalyst in the presence of alumoxane. This catalyst system is capable of producing polyethylene copolymers having a high degree of structural randomness and narrow molecular weight distribution. Also reported in EP 349,886 are references to prior amide containing Group IV-B metal catalysts for the homopolymerization of ethylene, which, when applied to copolymerization, suffer from the various disadvantages of low molecular weight product, broad molecular weight distribution and low catalytic activity.

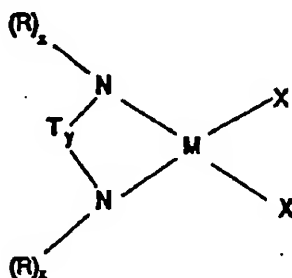
In view of the high strength and other physical properties that make stereoregular polymers desirable in applications for which other moldable plastics are ill suited and in view of the few methods currently available for producing stereoregular polymers, there is a need for a catalyst as disclosed hereinafter for producing high molecular weight, highly isotactic polymers. It is further desirable that such a catalyst have high activity so as to allow production of a polymer which is ready to be molded and/or machined for its ultimate use without treatment for removal of contaminants (catalyst residue). It is also desirable to obtain a catalyst that is useful for production of ethylene base polymers.

#### SUMMARY OF THE INVENTION

This invention discloses an alumoxane cocatalyzed catalyst system for the production of highly crystalline

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polyolefins the transition metal component of which is a bridged amido transition metal compound represented by the general formula:



wherein: "M" is zirconium, hafnium or titanium; "N" is  
 5 a nitrogen atom having three substituents; "y" is 1 or 0  
 denoting the presence or absence, respectively, of a  
 bridging group T between nitrogen atoms and "z" is 2 - y;  
 "X" and "X'" are any univalent anionic ligand such as a  
 halide, hydride, substituted or unsubstituted C<sub>1</sub>-C<sub>30</sub>  
 10 hydrocarbyl, alkoxide, aryloxy, amide, arylamide,  
 phosphide, arylphosphide, or "X" and "X'" together are a  
 divalent radical such as an alkylidene, cyclometallated  
 hydrocarbyl or any other divalent anionic chelating  
 ligand; "T" is a covalent bridging group selected from  
 15 the group consisting of unsubstituted hydrocarbyls and  
 hydrocarbyls containing a Group IV-A or VI-A element; and  
 each "R" and "R'" is independently a radical selected  
 from the group consisting of singly branched hydrocarbyl  
 radicals having between 1 and 30 carbon atoms, multiple  
 20 branched hydrocarbyl radicals having between 1 and 30  
 carbon atoms, halogen radicals, amido radicals, phosphido  
 radicals, silyl radicals, alkoxy radicals, alkylborido  
 radicals, C<sub>1</sub>-C<sub>30</sub> hydrocarbyl-substituted Group IV-A  
 metalloid radicals; and substituted C<sub>1</sub>-C<sub>30</sub> hydrocarbyl  
 25 radicals wherein one or more hydrogen atoms is replaced  
 by a halogen radical, an amido radical, a phosphido  
 radical, an alkoxy radical or any other radical  
 containing a Lewis acidic or basic functionality.

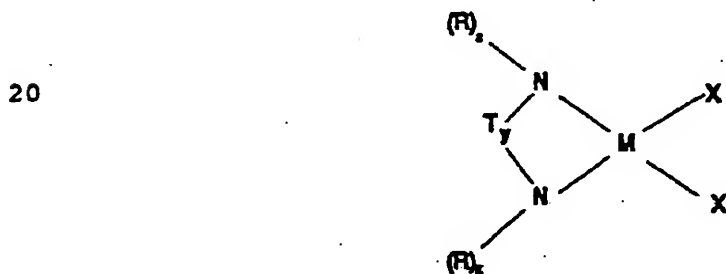
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Further disclosed is a polymerization process incorporating the catalyst system. The catalyst system is prepared by the combination of an amido transition metal compound and an alumoxane, and may be employed in solution, slurry, gas phase, or high pressure polymerization. The catalyst may also be prepared in the supported form. The catalyst system of this invention polymerizes propylene to high molecular weight, highly isotactic polypropylene, in addition to homopolymerizing ethylene and copolymerizing ethylene or propylene with  $\alpha$ -olefins, cyclic olefins, dienes or other unsaturated monomers.

#### DESCRIPTION OF THE PREFERRED EMBODIMENT

##### A. Transition Metal Component

The Group IV-B transition metal component of the catalyst system is represented by the general formula:



25

wherein the letter symbols have the following meanings:

"M" is zirconium, titanium or hafnium;

"N" is a nitrogen atom having three substituent groups;

"y" is 1 or 0 denoting the presence or absence, respectively, of a bridging group T between nitrogen atoms and "z" is 2 - y;

each "R" is independently a radical selected from the group consisting of singly branched hydrocarbyl

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radicals having between 1 and 30 carbon atoms, preferably between 3 and 30 carbon atoms; multiply branched hydrocarbyl radicals having between 1 and 30 carbon atoms, preferably between 3 and 30 carbon atoms; 5 halogen radicals; amido radicals; phosphido radicals; silyl radicals; alkoxy; and alkylborido radicals; substituted  $C_1-C_{30}$  hydrocarbyl radicals wherein one or more hydrogen atoms is replaced by a halogen radical, an amido radical, a phosphido radical, an alkoxy radical or 10 any other radical containing a Lewis acidic or basic functionality;  $C_1-C_{30}$  hydrocarbyl-substituted metalloid radicals wherein the metalloid is selected from the Group IV-A of the Periodic Table of Elements;

each "X" is independently any univalent anionic 15 ligand such as a halide, hydride, or substituted or unsubstituted  $C_1-C_{20}$  hydrocarbyl, alkoxide, aryloxy, amide, arylamide, phosphide, arylphosphide or both "X" and "X'" together are an alkylidene, a cyclometallated hydrocarbyl or any other divalent anionic chelating 20 ligand; more particularly, X may be a ligand of the general formula  $N(R)_2$  wherein R has the same meaning previously ascribed to it; most particularly, X may be a silylamide of the general formula  $N[Si(R)_3]_2$ ;

T is a covalent bridging group containing a Group 25 IV-A or VI-A element such as, but not limited to, a dialkyl, alkylaryl or diaryl silicon radical; a dialkyl, alkylaryl or diaryl germanium radical; alkyl or aryl phosphine; alkyl or aryl amine radical; an oxygen or sulfur radical; or a hydrocarbyl radical having 1 or more 30 carbon atoms such as methylene, ethylene and the like.

Specific, nonlimiting examples of the T group which are suitable as a constituent group of the Group IV-B transition metal component of the catalyst system are dimethylsilyl, diethylsilyl, di-n-propylsilyl, 35 diisopropylsilyl, di-n-butylsilyl, di-t-butylsilyl, di-n-

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hexylsilyl, methylphenylsilyl, ethylmethylsilyl, diphenylsilyl, di(p-t-butylphenethylsilyl), n-hexylmethylsilyl, cyclopentamethylenesilyl, cyclotetramethylenesilyl, cyclotrimethylenesilyl, 5 dimethylgermanyl, diethylgermanyl, methylene, dimethylmethylene, diethylmethylene, ethylene, dimethylethylene, diethylethylene, dipropylethylene, propylene, dimethylpropylene, diethylpropylene, 1,1-dimethyl-3,3-dimethylpropylene, tetramethyldisiloxane, 10 1,1,4,4-tetramethyldisilylethylene, oxygen and sulfur.

Exemplary hydrocarbyl radicals for X are methyl, ethyl, propyl, isopropyl, butyl, amyl, isoamyl, hexyl, isobutyl, heptyl, octyl, nonyl, decyl, cetyl, 2-ethylhexyl, phenyl and the like, with methyl being 15 preferred. Exemplary halogen atoms for X include chlorine, bromine, fluorine and iodine, with chlorine being preferred. Exemplary alkoxides and aryloxides for X are methoxide, ethoxide, propoxide, butoxide, phenoxide and substituted phenoxides such as 4-methylphenoxide. 20 Exemplary amides of X are dimethylamide, diethylamide, methylethylamide, di-t-butylamide, diisopropylamide and the like. Exemplary aryl amides are diphenylamide and any other substituted phenyl amides. Exemplary silyl amides are di-trimethylsilylamide, di-triethylsilylamide 25 and triethyl-trimethyl silylamide, with di-trimethylsilylamide being preferred. Exemplary phosphides of X are diphenylphosphide, dicyclohexylphosphide, diethylphosphide, dimethylphosphide and the like. Exemplary alkylidene radicals for both X's together are methylenidene, 30 ethylenidene, propylenidene, or the dianion of ethyleneglycol and the like.

Suitable hydrocarbyl and substituted hydrocarbyl radicals for the R group will contain from 1 to about 30 35 carbon atoms and include singly and multiply branched

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alkyl radicals, cyclic hydrocarbon radicals, alkyl-substituted cyclic hydrocarbon radicals, aromatic radicals and alkyl-substituted aromatic radicals, amido-substituted hydrocarbon radicals, phosphido-substituted hydrocarbon radicals, alkoxy-substituted hydrocarbon radicals, and halo-substituted hydrocarbon radicals or hydrocarbon radicals containing substitutions by any Lewis basic or acidic functional group. Suitable organometallic radicals for the R group include trimethylsilyl, triphenylsilyl, triphenylgermyl, trimethylgermyl and the like. Other suitable radicals for the R group include amido radicals, phosphido radicals, alkoxy radicals, alkyl boride radicals and the like. Of the suitable R groups the organometallic radicals of silicon such as trimethylsilyl, triethylsilyl, ethyldimethylsilyl and methyldiethylsilyl are preferred; the most preferred being trimethylsilyl.

A number of final components may be formed by permuting all possible combinations of the constituent moieties with each other. Illustrative transition metal compounds are: bis(di-trimethylsilylamido) zirconium dichloride, bis(di-isobutylamido) hafnium dimethyl, bis(di-tertbutylamido)zirconium dichloride, (di-cyclohexylamido)(di-trimethylsilylamido) titanium dihydride, tris(di-trimethylsilylamido) zirconium chloride, tris(di-triphenylgermylamido) hafnium chloride, and tetrakis(di-trimethylsilylamido) zirconium.

The Group IV-B metal compounds have been used to produce isotactic polypropylene of high stereoregularity. As demonstrated in example 9, when the achiral compound bis(di-trimethylsilylamido) zirconium dichloride is combined with alumoxane to form a catalyst system, that system is capable of producing isotactic polypropylene having fewer than 50 chain defects per 1000 monomer units. The preparation of compounds of this type are

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well known in the literature and include references such as R.A. Anderson, Inorganic Chemistry (1979), 18, 2928.

#### B. Alumoxane Component

5       The alumoxane component of the catalyst system is an oligomeric compound which may be represented by the general formula  $(R^3-Al-O)_m$  which is a cyclic compound, or may be  $R^4(R^5-Al-O)_m-AlR^6_2$  which is a linear compound. An alumoxane is generally a mixture of both the linear and cyclic compounds. In the general alumoxane formula 10  $R^3$ ,  $R^4$ ,  $R^5$  and  $R^6$  are, independently a  $C_1-C_5$  alkyl radical, for example, methyl, ethyl, propyl, butyl or pentyl and "m" is an integer from 1 to about 50. Most preferably,  $R^3$ ,  $R^4$ ,  $R^5$  and  $R^6$  are each methyl and "m" is at least 4. When an alkyl aluminum halide is employed in 15 the preparation of the alumoxane, one or more  $R^{3-6}$  groups may be halide.

As is now well known, alumoxanes can be prepared by various procedures. For example, a trialkyl aluminum may 20 be reacted with water, in the form of a moist inert organic solvent; or the trialkyl aluminum may be contacted with a hydrated salt, such as hydrated copper sulfate suspended in an inert organic solvent, to yield an alumoxane. Generally, however prepared, the reaction 25 of a trialkyl aluminum with a limited amount of water yields a mixture of both linear and cyclic species of alumoxane.

Suitable alumoxanes which may be utilized in the catalyst systems of this invention are those prepared by 30 the hydrolysis of a trialkylaluminum or haloalkylaluminum; such as trimethylaluminum, triethylaluminum, tripropylaluminum; triisobutylaluminum, dimethylaluminumchloride, diisobutylaluminumchloride, diethylaluminumchloride, and the like. Th most preferred 35 alumoxane for use is methylalumoxane (MAO).



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Methylalumoxanes having an average degree of oligomerization of from about 4 to about 25 ("m" = 4 to 25), with a range of 13 to 25, are the most preferred.

5           C. Catalyst System

The catalyst systems employed in the invention comprise a complex formed upon admixture of the amido Group IV-B transition metal component with an alumoxane component. The catalyst system may be prepared by  
10 addition of the requisite bis-amido Group IV-B transition metal and alumoxane components to an inert solvent in which olefin polymerization can be carried out by a solution, slurry or bulk phase polymerization procedure.

The catalyst system may be conveniently prepared by  
15 placing the selected amido Group IV-B transition metal component and the selected alumoxane component, in any order of addition, in an alkane or aromatic hydrocarbon solvent -- preferably one which is also suitable for service as a polymerization diluent. Where the  
20 hydrocarbon solvent utilized is also suitable for use as a polymerization diluent, the catalyst system may be prepared in situ in the polymerization reactor. Alternatively, the catalyst system may be separately prepared, in concentrated form, and added to the  
25 polymerization diluent in a reactor. Or, if desired, the components of the catalyst system may be prepared as separate solutions and added to the polymerization diluent in a reactor, in appropriate ratios, as is suitable for a continuous liquid phase polymerization  
30 reaction procedure. Alkane and aromatic hydrocarbons suitable as solvents for formation of the catalyst system and also as a polymerization diluent are exemplified by, but are not necessarily limited to, straight and branched chain hydrocarbons such as isobutane, butane, pentane,  
35 hexane, heptane, octane and the like, cyclic and

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alicyclic hydrocarbons such as cyclohexane, cycloheptane, methylcyclohexane, methylcycloheptane and the like, and aromatic and alkyl-substituted aromatic compounds such as benzene, toluene, xylene and the like. Suitable solvents  
5 also include liquid olefins which may act as monomers or comonomers including ethylene, propylene, 1-butene, 1-hexene and the like.

In accordance with this invention optimum results are generally obtained wherein the amido Group IV-B  
10 transition metal compound is present in the polymerization diluent in a concentration of from about 0.0001 to about 1.0 millimoles/liter of diluent and the alumoxane component is present in an amount to provide a molar aluminum to transition metal ratio of from about  
15 1:1 to about 20,000:1. Sufficient solvent should be employed so as to provide adequate heat transfer away from the catalyst components during reaction and to permit good mixing.

The catalyst system ingredients -- that is, the  
20 amido Group IV-B transition metal, the alumoxane, and polymerization diluent -- can be added to the reaction vessel rapidly or slowly. The temperature maintained during the contact of the catalyst components can vary widely, such as, for example, from -10° to 300°C. Greater  
25 or lesser temperatures can also be employed. Preferably, during formation of the catalyst system, the reaction is maintained within a temperature of from about 25° to 100°C, most preferably about 25°C.

At all times, the individual catalyst system  
30 components, as well as the catalyst system once formed, are protected from oxygen and moisture. Therefore, the reactions to prepare the catalyst system are performed in an oxygen and moisture free atmosphere and, where the catalyst system is recovered separately it is recovered  
35 in an oxygen and moisture free atmosphere. Preferably,

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therefore, the reactions are performed in the presence of an inert dry gas such as, for example, helium or nitrogen.

5     D.     Polymerization Process

          In a preferred embodiment of the process of this invention the catalyst system is utilized in the liquid phase (slurry, solution, suspension or bulk phase or combination thereof), high pressure fluid phase or gas  
10     phase polymerization of an olefin monomer. These processes may be employed singularly or in series. The liquid phase process comprises the steps of contacting an olefin monomer with the catalyst system in a suitable polymerization diluent and reacting said monomer in the  
15     presence of said catalyst system for a time and at a temperature sufficient to produce a polyolefin of high molecular weight.

          The monomer for such process may comprise propylene alone, for the production of a isotactic polypropylene.  
20     Conditions most preferred for the production of isotactic polypropylene are those wherein propylene is submitted to the reaction zone at pressures of from about 0.019 psi to about 50,000 psi and the reaction temperature is maintained at from about -100° to about 300°C. The  
25     aluminum to transition metal molar ratio is preferably from about 1:1 to 20,000:1. A more preferable range would be 1:1 to 2000:1. The reaction time is preferably from about 1 hour to about 6 hours.

          The monomer may also comprise ethylene alone, for  
30     the production of homopolyethylene, or ethylene in combination with an  $\alpha$ -olefin having 3 to 20 carbon atoms for the production of an ethylene- $\alpha$ -olefin copolymer. Homopolymers of higher  $\alpha$ -olefin such as butene and copolymers thereof with ethylene and/or C<sub>4</sub> or higher  
35      $\alpha$ -olefins and diolefins can also be prepared. Conditions

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most preferred for the homo- or copolymerization of ethylene are those wherein ethylene is submitted to the reaction zone at pressures of from about 0.019 psi to about 50,000 psi and the reaction temperature is maintained at from about -100° to about 300°C. The aluminum to transition metal molar ratio is preferably from about 1:1 to 20,000:1. A more preferable range would be 1:1 to 2000:1. The reaction time is preferably from about 10 seconds to about 1 hour.

Without limiting in any way the scope of the invention, one means for carrying out the process of the present invention for production of a copolymer is as follows: in a stirred-tank reactor, liquid  $\alpha$ -olefin monomer is introduced, such as 1-butene. The catalyst system is introduced via nozzles in either the vapor or liquid phase. Feed ethylene gas is introduced either into the vapor phase of the reactor, or sparged into the liquid phase as is well known in the art. The reactor contains a liquid phase composed substantially of liquid  $\alpha$ -olefin comonomer, together with dissolved ethylene gas, and a vapor phase containing vapors of all monomers. The reactor temperature and pressure may be controlled via reflux of vaporizing  $\alpha$ -olefin monomer (autorefrigeration), as well as by cooling coils, jackets etc. The polymerization rate is controlled by the concentration of catalyst. The ethylene content of the polymer product is determined by the ratio of ethylene to  $\alpha$ -olefin comonomer in the reactor, which is controlled by manipulating the relative feed rates of these components to the reactor.

#### EXAMPLES

##### Example 1

The polymerization run was performed in a 1-liter autoclave reactor equipped with a paddle stirrer, an

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external water jacket for temperature control, a regulated supply of dry nitrogen, ethylene, propylene, 1-butene and hexane, and a septum inlet for introduction of other solvents or comonomers, transition metal compound and alumoxane solutions. The reactor was dried and degassed thoroughly prior to use. A typical run consisted of injecting 400 ml of toluene, 5 ml 1.0 M MAO, 0.27 mg of  $[(\text{Me}_3\text{Si})_2\text{N}]_2\text{ZrCl}_2$  (0.2 ml of a 13.5 mg in 10 ml of toluene solution) into the reactor. The reactor was then heated to 80°C and the ethylene (60 psi) was introduced into the system. The polymerization reaction was limited to 10 minutes. The reaction was ceased by rapidly cooling and venting the system. The solvent was evaporated off of the polymer by a stream of nitrogen. Polyethylene was recovered (7.4 g, MW = 315,000, MWD = 2.261).

#### Example 2

Using the same reactor design and general procedure as example 1, 400 ml of toluene, 5.0 ml of 1.0 M MAO, and 0.32 mg of  $[(\text{Me}_3\text{Si})_2\text{N}]_2\text{HfCl}_2$  (0.2 ml of a 1.60 mg in 10 ml of toluene solution) were added to the reactor. The reactor was heated at 80°C, the ethylene was introduced (60 psi), and the reaction was allowed to run for 10 minutes, followed by rapidly cooling and venting the system. After evaporation of the toluene, 2.7 g of polyethylene was recovered (MW = 267,200, MWD = 2.122).

#### Example 3

Using the same reactor design and general procedure as example 1, 300 ml of toluene, 100 ml of propylene, 7.0 ml of 1.0 M MAO, and 1.35 mg of  $[(\text{Me}_3\text{Si})_2\text{N}]_2\text{ZrCl}_2$  (1 ml of a 13.5 mg in 10 ml of toluene solution) were added to the reactor. The reactor was heated at 50°C, the ethylene was introduced (65 psi), and the reaction was allowed to run for 30 minutes, followed by rapidly cooling and venting the system. After evaporation of the

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toluene, 9.3 g of an ethylene-propylene copolymer was recovered (MW = 131,000, MWD = 1.837, 121.7 short chain branches (SCB)/1000C by IR).

#### Example 4

5           Using the same reactor design and general procedure as example 1, 300 ml of toluene, 100 ml of propylene, 7.0 ml of 1.0 M MAO, and 1.6 mg of  $[(\text{Me}_3\text{Si})_2\text{N}]_2\text{HfCl}_2$  (1 ml of a 16 mg in 10 ml of toluene solution) were added to the reactor. The reactor was heated at 80°C, the ethylene  
10           was introduced (60 psi), and the reaction was allowed to run for 30 minutes, followed by rapidly cooling and venting the system. After evaporation of the toluene, 8.2 g of an ethylene-propylene copolymer was recovered (MW = 80,700, MWD = 1.537, 89.3 SCB/1000C by IR).

#### 15           Example 5

          Using the same reactor design and general procedure as example 1, 300 ml of toluene, 100 ml of 1-butene, 7.0 ml of 1.0 M MAO, and 1.35 mg of  $[(\text{Me}_3\text{Si})_2\text{N}]_2\text{ZrCl}_2$  (1 ml of a 13.5 mg in 10 ml of toluene solution) were added to  
20           the reactor. The reactor was heated at 80°C, the ethylene was introduced (60 psi), and the reaction was allowed to run for 30 minutes, followed by rapidly cooling and venting the system. After evaporation of the toluene, 4.3 g of an ethylene-butene copolymer was  
25           recovered (MW = 91,100, MWD = 1.643, 51.4 SCB/1000C by  $^{13}\text{C}$  NMR).

#### Example 6

          Using the same reactor design and general procedure as example 1, 300 ml of toluene, 100 ml of 1-butene, 7.0  
30           ml of 1.0 M MAO, and 1.6 mg of  $[(\text{Me}_3\text{Si})_2\text{N}]_2\text{HfCl}_2$  (1 ml of a 16 mg of 10 ml of toluene solution) were added to the reactor. The reactor was heated at 80°C, the ethylene  
          was introduced (60 psi), and the reaction was allowed to run for 30 minutes, followed by rapidly cooling and  
35           venting the system. After evaporation of the toluene,

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9.3 g of an ethylene-butene copolymer was recovered (MW = 70,800, MWD = 1.710, 46.8 SCB/1000C by  $^{13}\text{C}$  NMR).

Example 7

Using the same reactor design and general procedure as example 1, 300 ml of toluene, 100 ml of 1-hexene, 7.0 ml of 1.0 M MAO, and 1.35 mg of  $[(\text{Me}_3\text{Si})_2\text{N}]_2\text{ZrCl}_2$  (1 ml of a 13.5 mg in 10 ml of toluene solution) were added to the reactor. The reactor was heated at 80°C, the ethylene was introduced (60 psi), and the reaction was allowed to run for 30 minutes, followed by rapidly cooling and venting the system. After evaporation of the toluene, 13.9 g of an ethylene-hexene copolymer was recovered (MW = 111,200, MWD = 1.782, 32.2 SCB/1000C by IR).

Example 8

Using the same reactor design and general procedure as example 1, 300 ml of toluene, 100 ml of 1-hexene, 7.0 ml of 1.0 M MAO, and 1.6 mg of  $[(\text{Me}_3\text{Si})_2\text{N}]_2\text{HfCl}_2$  (1 ml of a 16.0 mg in 10 ml of toluene solution) were added to the reactor. The reactor was heated at 50°C, the ethylene was introduced (65 psi), and the reaction was allowed to run for 30 minutes, followed by rapidly cooling and venting the system. After evaporation of the toluene, 8.7 g of an ethylene-hexene copolymer was recovered (MW = 236,700, MWD = 1.780, 20.1 SCB/1000C by IR).

Example 9

Using the same reactor design and general procedure as example 1, 100 ml of toluene, 200 ml of propylene, 10.0 ml of 1.0 M MAO, and 8.3 mg of  $[(\text{Me}_3\text{Si})_2\text{N}]_2\text{ZrCl}_2$  in 10 ml toluene were added to the reactor. The reactor was heated at 30°C and the reaction was allowed to run for 3 hours, followed by rapidly cooling and venting the system. After evaporation of the toluene, 3.2 g of isotactic polypropylene was recovered (MW = 95,500, MWD =

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1.758, 90% (m) isotactic with 40 chain defects per 1000 monomer units as determined by  $^{13}\text{C}$  NMR, 146°C mp).

#### Example 10

The polymerization was performed in a stirred 100 ml stainless steel autoclave which was equipped to perform polymerizations at temperatures up to 300°C and pressures up to 2500 bar. the reactor was evacuated, purged with nitrogen, purged with ethylene and heated to 202°C. The comonomer, 1-hexene (75 ml), was added to the reactor under ethylene pressure. A stock solution of  $[(\text{Me}_3\text{Si})_2\text{N}]_2\text{ZrCl}_2$  was prepared by dissolving 7.6 mg of the transition metal compound in 25 ml of toluene. The test solution was prepared by adding 2.5 ml of the stock solution to 10.0 ml of a 1.0 M MAO solution. The test solution (0.43 ml) was transferred by nitrogen pressure into a constant-volume injection tube. The autoclave was pressurized with ethylene to 1792 bar and was stirred at 1800 rpm. The test solution (0.43 ml) was injected into the autoclave with excess pressure, at which time a temperature rise of 9°C was observed. The temperature and pressure were recorded continuously for 120 seconds, at which time the contents of the autoclave were rapidly vented into a receiving vessel. The reactor was washed with xylene to recover any polymer remaining within. These washings were combined with the polymer released when the reactor was vented. Precipitation of the polymer from the mixture by addition of acetone yielded 1.3 g of an ethylene-hexene copolymer (MW = 42,000, MWD = 2.07, 8.9 SCB/1000C by IR).

#### Example 11

Using the same reactor design as described in example 10, the reactor was evacuated, purged with nitrogen, purged with ethylene and heated to 199°C. The comonomer 1-hexene (75 ml), was added to the reactor under ethylene pressure. A stock solution of



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5  $[(\text{Me}_3\text{Si})_2\text{N}]_2\text{HfCl}_2$  was prepared by dissolving 9.0 mg of the transition metal compound in 25 ml of toluene. The test solution was prepared by adding 2.5 ml of the stock solution to 10.0 ml of a 1.0 M MAO solution. The test  
10 solution (0.43 ml) was transferred by nitrogen pressure into a constant-volume injection tube. The autoclave was pressurized with ethylene to 1831 bar and was stirred at 1800 rpm. The test solution was injected into the autoclave with excess pressure, at which time a  
15 temperature rise of 7°C was observed. The temperature and pressure were recorded continuously for 120 seconds, at which time the contents of the autoclave were rapidly vented into a received vessel. The reactor was washed with xylene to recover any polymer remaining within. These washings were combined with the polymer released when the reactor was vented. Precipitation of the polymer from the mixture by addition of acetone yielded 0.5 g of an ethylene-hexene copolymer (MW = 57,000, MWD = 2.22, 8.0 SCB/1000C by IR).

TABLE A

EXAMPLE NUMBER	COMPOUND*	CATALYST			REACTOR			POLYMER PRODUCT			
		TRANSITION METAL COMPOUND ("TMC") ( $\mu$ moles)	ALUOXANE ("NAO") ( $\mu$ moles)	CATALYTIC EFFICIENCY (g POLYMER/ $\mu$ mole TMC)	MONOMER/COMONOMER	ETHYLENE PRESSURE (PSI)	TEMPERATURE ( $^{\circ}$ C)	YIELD (g)	MOLECULAR WEIGHT (g/mole)	MOLECULAR WEIGHT DISTRIBUTION	SCB/1000 $^{\circ}$ C
1	Zr	0.56	5000	13.2	ETHYLENE	60	80	7.4	315,100	2.261	---
2	Hf	0.56	5000	4.8	ETHYLENE	60	80	2.4	267,200	2.122	---
3	Zr	7.81	7000	3.3	ETHYLENE/PROPYLENE	60	50	9.3	131,100	1.837	121.7 <sup>d</sup>
4	Hf	2.81	7000	2.9	ETHYLENE/PROPYLENE	60	80	8.2	80,700	1.537	89.3 <sup>d</sup>
5	Zr	2.81	7000	1.5	ETHYLENE/1-BUTENE	60	80	4.3	91,100	1.643	51.4 <sup>c</sup>
6	Hf	2.81	7000	3.3	ETHYLENE/1-BUTENE	60	80	9.3	70,800	1.710	46.8 <sup>c</sup>
7	Zr	2.81	7000	4.9	ETHYLENE/1-HEXENE	60	80	13.9	111,300	1.782	32.2 <sup>c</sup>
8	Hf	2.81	7000	3.1	ETHYLENE/1-HEXENE	65	50	8.7	236,700	1.780	20.0 <sup>d</sup>
9	Zr	17.3	10000	0.2	PROPYLENE	---	30	3.2 <sup>b</sup>	95,500	1.758	---
10	Zr	1.58	4300	0.8	ETHYLENE/1-HEXENE	2.6x10 <sup>4</sup>	202	1.3	42,000	2.07	8.9 <sup>d</sup>
11	Hf	1.56	4300	0.3	ETHYLENE/1-HEXENE	2.7x10 <sup>4</sup>	199	0.5	51,000	2.22	8.0 <sup>d</sup>

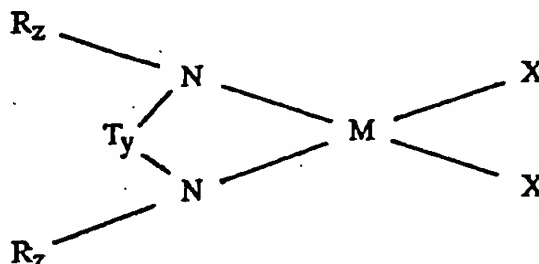
\* The transition metal catalyst components of the examples are zirconium and hafnium species of  $((\text{Me}_3\text{Si})_2\text{N})_2\text{MCl}_2$ .  
 b 90% isotactic polypropylene having 40 defects per 1000 monomer units (determined by  $^{13}\text{C}$  NMR) was produced.  
 c Determined by  $^{13}\text{C}$  NMR.  
 d Determined by IR.

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5       The invention has been described with reference to  
its preferred embodiments. Those of ordinary skill in  
the art may, upon reading this disclosure, appreciate  
changes or modifications which do not depart from the  
scope and spirit of the invention as described above or  
claimed hereafter.

Claims:

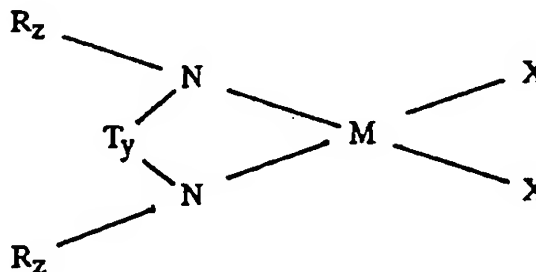
A compound represented by the general formula:



wherein: "y" is 1 denoting the presence of a bridging group T between nitrogen atoms; "z" is 2 - y; "M" is zirconium, hafnium or titanium; "N" is a nitrogen atom having three substituents; each "X" is, independently, any univalent anionic ligand such as a halide, hydride, substituted or unsubstituted C<sub>1</sub>-C<sub>30</sub> hydrocarbyl, alkoxide, aryloxy, amide, arylamide, phosphide, or arylphosphide; "T" is a covalent bridging group selected from the group consisting of unsubstituted hydrocarbyls and substituted hydrocarbyls containing a Group IV-A or VI-A element; and each "R" is, independently, a radical selected from the group consisting of singly branched hydrocarbyl radicals having between 4 and 30 carbon atoms, multiply branched hydrocarbyl radicals having between 4 and 30 carbon atoms, halogen radicals, amido radicals, phosphido radicals, silyl radicals, alkoxy radicals, alkylborido radicals, C<sub>1</sub>-C<sub>30</sub> hydrocarbyl-substituted Group IV-A metalloid radicals; and substituted C<sub>1</sub>-C<sub>30</sub> hydrocarbyl radicals wherein one or more hydrogen atoms is replaced by a halogen radical, an amino radical, a phosphido radical, an alkoxy radical or any other radical containing a Lewis acidic or basic functionality.

2. A catalyst system for the polymerization of alpha olefins comprising:

a) The compound of claim 1 or a compound of the general formula:



wherein: "y" is 1 or 0 denoting the presence or absence, respectively, of a bridging group T between nitrogen atoms; "z" is 2 - y; "M" is zirconium, hafnium, or titanium; "N" is a nitrogen atom having three substituents; each "X" is, independently, any univalent anionic ligand such as a halide, hydride, substituted or unsubstituted C<sub>1</sub>-C<sub>30</sub> hydrocarbyl, alkoxide, aryloxy, amide, arylamide, phosphide or arylphosphide; "T" is a covalent bridging group selected from the group consisting of unsubstituted hydrocarbyls and substituted hydrocarbyls containing a Group IV-A or VI-A element; and each "R" is, independently, a radical selected from the group consisting of singly branched hydrocarbyl radicals having between 4 and 30 carbon atoms, multiply branched hydrocarbyl radicals having between 4 and 30 carbon atoms, halogen radicals, amido radicals, phosphido radicals, silyl radicals, alkoxy radicals, alkylborido radicals, C<sub>1</sub>-C<sub>30</sub> hydrocarbyl-substituted Group IV-A metalloid radicals; and substituted C<sub>1</sub>-C<sub>30</sub> hydrocarbyl radicals wherein one or more hydrogen atoms is replaced by a halogen radical, an amido radical, a phosphido radical, an alkoxy radical or any other radical containing a Lewis acidic or basic functionality; and

b) an alumoxane.

3. The compound of claim 1 or system of claim 2 wherein each R is, independently, a radical selected from the group consisting of halogen radicals, amido radicals, phosphido radicals, silyl radicals, alkoxy radicals, alkylborido radicals, C<sub>1</sub>-C<sub>30</sub> hydrocarbyl-substituted Group IV-A metalloid radicals; and substituted C<sub>1</sub>-C<sub>30</sub> hydrocarbyl radicals wherein one or more hydrogen atoms is replaced by a halogen radical, an amido radical, a phosphido radical, an alkoxy radical or any other radical containing a Lewis acidic or basic functionality.

4. The compound or system of claim 1, 2, or 3 wherein "T" is a covalent bridging group containing a Group IV-A atom.

5. The compound or system of any preceding claim wherein at least one "R" is a silicon containing radical.

6. The compound or system of any preceding claim wherein at least one "X" is a nitrogen containing radical.

7. The compound or system of any preceding claim wherein each "X" is, independently, selected from the group consisting of hydrides, alkoxides, amides, hydrocarbyls and halides.

8. The compound or system of claim 7 wherein at least one "X" is selected from the group consisting of hydrides, hydrocarbyls, amidos, and halides.

9. The compound or system of any preceding claim wherein "M" is zirconium or hafnium.

10. The catalyst system of any of claims 2-11 wherein the alumoxane is derived from the hydrolysis of an aluminumalkyl selected from the group consisting of trimethylaluminum, triethylaluminum, and triisobutylaluminum.

11. The catalyst system of any of claims 2-15 wherein the aluminum:transition metal ratio is from 1:1 to 20,000:1.

12. A process for producing poly alpha-olefin comprising the steps of:

a) contacting alpha-olefin monomer or monomers with a catalytically active combination comprising the compound or system of any preceding claim, and

b) recovering poly alpha-olefin.

13. The process of claim 12 wherein the poly alpha-olefin produced is isotactic polypropylene, the monomer of a) is propylene.

14. The process of claim 12 wherein the poly alpha-olefin produced is polyethylene or a copolymer of ethylene and another alpha-olefin having 3-20 carbon atoms, the monomer of a) comprising ethylene or ethylene and another alpha-olefin having 3 to 20 carbon atoms.

15. The process of claim 12, 13, or 14 wherein the polymerization reaction time is between 1 and 6 hours and/or the reaction

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pressure is from 0.13 kPa (0.019 psi) to 344.75 MPa (50,000 psi) and/or the reaction temperature is maintained between -100° C and 300° C.

16. The process of claim 15 wherein the polymer produced has MWD in the range of 1.5-3.

17. The process of claim 15 or 16 wherein the polymer produced has SCB in the range of 5-150.

## INTERNATIONAL SEARCH REPORT

International Application No.

PCT/US 91/09676

<b>I. CLASSIFICATION OF SUBJECT MATTER</b> (If several classification symbols apply, indicate all) *		
According to International Patent Classification (IPC) or to both National Classification and IPC		
IPC <sup>5</sup> : C 07 F 7/00, C 08 F 4/642, C 08 F 10/00		
<b>II. FIELDS SEARCHED</b>		
Minimum Documentation Searched *		
Classification System	Classification Symbols	
IPC <sup>5</sup>	C 07 F, C 08 F	
Documentation Searched other than Minimum Documentation to the extent that such Documents are included in the Fields Searched *		
<b>III. DOCUMENTS CONSIDERED TO BE RELEVANT *</b>		
Category *	Citation of Document, ** with indication, where appropriate, of the relevant passages **	Relevant to Claim No. **
X	ORGANOMETALLICS, vol. 2, no. 1, January 1983, pages 16-20, R.P. PLANALP et al. "Dialkyl Bis(bis(trimethylsilyl)amido) Group 4A Metal Complexes", see pages 19-20, Experimental Section.	1
X	ZEITSCHRIFT FÜR ANORGANISCHE UND ALLGEMEINE CHEMIE, vol. 459, December 1979, pages 111-118, H. BÜRGER, D. BEIERSDORF "Cyclische Titanamide mit Sila-titana- -diazacyclobutan-Struktur", see page 118, table 3.	1
X	JOURNAL OF ORGANOMETALLIC CHEMISTRY, vol. 192, 1980, pages 189-193, R.A. ANDERSEN "Dialkylbis(bis(trimethyl-	1
<p>* Special categories of cited documents: **</p> <p>"A" document defining the general state of the art which is not considered to be of particular relevance</p> <p>"E" earlier document but published on or after the international filing date</p> <p>"L" document which may throw doubts on priority claim(s) or which is cited to establish the publication date of another citation or other special reason (as specified)</p> <p>"O" document referring to an oral disclosure, use, exhibition or other means</p> <p>"P" document published prior to the international filing date but later than the priority date claimed</p> <p>"T" later document published after the international filing date or priority date and not in conflict with the application but cited to understand the principle or theory underlying the invention</p> <p>"X" document of particular relevance; the claimed invention cannot be considered novel or cannot be considered to involve an inventive step</p> <p>"Y" document of particular relevance; the claimed invention cannot be considered to involve an inventive step when the document is combined with one or more other such documents, such combination being obvious to a person skilled in the art</p> <p>"Z" document member of the same patent family</p>		
<b>IV. CERTIFICATION</b>		
Date of the Actual Completion of the International Search	Date of Mailing of this International Search Report	
01 April 1992	16. 04. 92	
International Searching Authority	Signature of Authorized Officer	
EUROPEAN PATENT OFFICE	Daniella van der Haas	



III. DOCUMENTS CONSIDERED TO BE RELEVANT (CONTINUED FROM THE SECOND SHEET)		
Category *	Citation of Document, " with indication, where appropriate, of the relevant passages	Relevant to Claim No.
	<p>silyl)amido)hafnium(IV);            Unsymmetrical Dialkyl and            Alkyloxide Derivatives",            see pages 190-193,            Experimental.</p> <p>---</p>	
X	<p>INORGANIC CHEMISTRY, vol. 18,            December 1979, pages            2928-2932, R.A. ANDERSEN            "Dialkylbis(bis(trimethyl-            silyl)amido)zirconium(IV) and            -hafnium(IV).",            see page 2931, Experimental            Section.</p> <p>---</p>	1
A	<p>US, A, 4 774 301            (CAMPBELL Jr. et al.)            27 September 1988 (27.09.88),            see claim 1.</p> <p>----</p>	2

**ANHANG**

zum internationalen Recherchen-  
bericht über die internationale  
Patentanmeldung Nr.

**ANNEX**

to the International Search  
Report to the International Patent  
Application No.

**ANNEXE**

au rapport de recherche inter-  
national relatif à la demande de brevet  
international n°

PCT/US 91/09676 SAE 55987

In diesem Anhang sind die Mitglieder  
der Patentfamilien der in obenge-  
nannten internationalen Recherchenbericht  
angeführten Patentdokumente angegeben.  
Diese Angaben dienen nur zur Unter-  
richtung und erfolgen ohne Gewähr.

This Annex lists the patent family  
members relating to the patent documents  
cited in the above-mentioned inter-  
national search report. The Office is  
in no way liable for these particulars  
which are given merely for the purpose  
of information.

La présente annexe indique les  
membres de la famille de brevets  
relatifs aux documents de brevets cités  
dans le rapport de recherche inter-  
national visée ci-dessus. Les renseigne-  
ments fournis sont donnés à titre indica-  
tif et n'engagent pas la responsabilité  
de l'Office.

In Recherchenbericht angeführtes Patentdokument Patent document cited in search report Document de brevet cité dans le rapport de recherche	Datum der Veröffentlichung Publication date Date de publication	Mitglied(er) der Patentfamilie Patent family member(s) Membre(s) de la famille de brevets	Datum der Veröffentlichung Publication date Date de publication
US A - 4774301	27-09-88	keine - none - rien	